



**Wheelabrator
Air Pollution Control Inc.**

World Pollution Control Association

Wet Electrostatic Precipitation
Technology for the Utility Industry

By

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Acknowledgments

- Pilot Host Sites
 - First Energy's Bruce Mansfield Plant
 - Southern Company's Alabama Power's Plant Miller
- R&D Funding
 - DOE's NETL Office
 - Electric Power Research Institute
- Co-Authors
 - Wayne Buckley & Patrick Doonan- WAPC
 - Dr. Ralph Altman – EPRI



Outline

- Control Technologies
- WESP History
- Compare to Dry ESP
- How WESP work
- Why WESP
- What is PM_{2.5}
- Opacity
- Applications
- Removal Performance
- Types of Wet ESPs
- Washing Options
- Design Parameters
- Materials
- Utility Installations
- Configurations
- Mercury Control
- New Developments
- Benefits



Overview- Control Technologies

Technology	Type	NO _x	PM ₁₀	SO ₂	Hg	PM _{2.5}	SO ₃
Low-NO _x Burners	dry	X					
SCR	dry	X					
SNCR	dry	X					
Dry ESP	dry		X			X	
Fabric Filter	dry		X			X	
SDA + FF	dry		X	X	X	X	X
Injection+FF	dry				X	X	X
FGD Scrubber	wet		X	X	X		X
Injection + FGD	wet			X	X		X
WESP	wet				X	X	X



WESP History

- First ESP was Wet , not Dry !
- Developed by Dr. Cottrell in 1907
- First dry ESP was 1922 at Detroit Edison
- Used to Control Sulfuric Acid Mist
- Numerous Industrial Applications
- Utility Installations are limited
- New PM2.5 Regulations may require WESP



Wet ESP vs. Dry ESP

OPERATIONAL ISSUES	DRY ESP	WET ESP
BACK CORONA	YES	NO
RE-ENTRAINMENT	YES	NO
PM10 REMOVAL	YES	NO
PM2.5 REMOVAL	Limited	YES
SO3 REMOVAL	NO	YES
MERCURY REMOVAL	NO	YES
OPACITY REDUCTION	NO	YES
WASTE WATER TREATMENT	NO	YES

A WESP DOES NOT REPLACE A DRY ESP



Wet Precipitation Process

A 3- Step Process

1. Charging – gas ions created by corona from discharge electrode charge flue gas particles.
2. Collection- the charged particles/mists are attracted to the oppositely charged collection electrode surface.
3. Cleaning – the collected particles/mists are washed away by water, preventing build-up on the collection surface.



Why Wet ESP?

- Multi-Pollutant Control
- Opacity Reduction <10%
 - SO₃ – up to 99%
 - PM2.5 – up to 99%
- Metals – up to 99%
- Mercury – depends on species

A Final Polishing Device



Typical Size of Various Particles

LOWER LIMIT OF VISIBILITY (NAKED EYE)...	40 MICRONS
WHITE BLOOD CELLS	25 MICRONS
RED BLOOD CELLS	8 MICRONS
BACTERIA (COCCI)	2 MICRONS
SULFURIC ACID MIST.....	0.3 MICRONS



Fine & Course Particles

- Course Particles
 - 2.5 to 50 micron in size
 - 10 micron is largest fraction
 - Mechanical, windblown & biological dust

- Fine Particles
 - 0.1 to 2.5 micron in size
 - 0.5 micron is largest fraction
 - Combustion particles
 - Most harmful due to being respirable



OPACITY

- Function of Light Extinction
- 0.5 micron particles are worst actors
- In-line opacity monitors give false reading
- Atmosphere condenses vapors into fine particles & mists
- FGD will also condense fines before stack
- Presence of SCR may also increase SO₃ concentration



EPA Chart- Pressure Drop vs. PM Removal Efficiency In a Wet Particulate Scrubber

90% removal = 25" w.c.

95% removal = 35" w.c.

99% removal = 50" w.c.



Industrial Applications

- Chemical
- Textile/Carpet
- Food Processing
- Mining
- Steel
- Glass
- Pharmaceutical
- Petro-Chemical
- Fiber Optics
- Hazardous Waste
- Soil Remediation
- Sulfuric Acid Production
- Arson Forensics
- Wood Products
- Medical Sterilization
- Automotive



Removal Capability

Eastman Chemical, TN Hazardous Waste Incineration

Pollutant	Units	Test Runs	MACT Limits	%
Particulate	gr/dscf, 7% O ₂	0.0024-0.0030	0.015	99.94
HCL/Cl ₂	ppmdv,	2.96-4.84	77	99.95
Chromium	ug/dscm	39.7-42.8	97	99.97
Lead	ug/dscm	3.59-3.85	240	99.95
Mercury	ug/dscm	1.82-1.98	130	79%
Dioxin/furan	ng TEQ/dscm	0.0131-0.0892	0.4	N/D



Removal Capability

Kyanite Mining, Willis Mountain, VA. Ore Roasting

Pollutant	Units	Inlet	Outlet	%
SO ₂	ppm	3,580	21.4	99.4
ACID MIST (H ₂ SO ₄)	gr /dscf	0.228	0.0159	93.0
PM2.5	gr/dscf	1.6	0.006	99.6
CONDENSED, INORGANIC	gr/dscf	0.1310	0.0143	89
CONDENSED, ORGANIC	gr/dscf	0.1415	0.0157	90
OPACITY		> 50%	<5%	



Types of Wet ESPs

- Tubular Type
 - Vertical Flow
 - Up-Flow
 - Down-flow

- Plate Type
 - Vertical Flow
 - Horizontal Flow



Washing Options

- On-line Options
 - Condensing – cooling jacket
 - Irrigated
- Off-Line Sprays
 - Intermittent Operation



Design Factors

- Particulate & Droplet Concentration and Size
- Velocity of the Gas
- Collection Surface Area
- Operating Voltage and Current
- Modular - limited by size of transformer
- Multiple Fields
 - In series- > % removal
 - In parallel > air flow



Operational Benefits

- 1/2" w.c. Pressure Drop
- No Additional Real Estate Possible
- Secondary Waste Treated & Concentrated
- Modular Design for Scale-Up
- Low Maintenance- No Moving Parts



Materials of Construction

- Materials can be:
 - Stainless Steel
 - 304L-316L-317LMN
 - Duplex Stainless
 - 904L, RA2205
 - Super Austenitic SS
 - A16XN, SMO254
 - High Nickel
 - C-276, C2000
 - Non-Metallic
 - Plastic or FRP- risk of fire
 - Membrane-risk of stretching/fire/plugging
- Dependent upon
 - SO₃ in flue gas
 - Dry-wet zones
 - Chloride levels in the water



Waste Water & Power Levels

- Water
 - If FGD present- first use
 - Service Water OK
 - If no water treatment present
 - Sluice to pond or
 - Install treatment system with recycle
 - Concentrate & remove wastes from water
- Power Requirements
 - Operating = @ 1kw /MW
 - Less than 1/2% plant power



WESP Utility Installations

- Japan – @ 30 installations
- Europe- @ ??
- North America
 - AES Deepwater - 1977
 - Xcel Energy's Sherco Station-1995
 - Dakota Gasification Co.-2003
 - New Brunswick Power- Coleson Cove -2004



Utility Applications

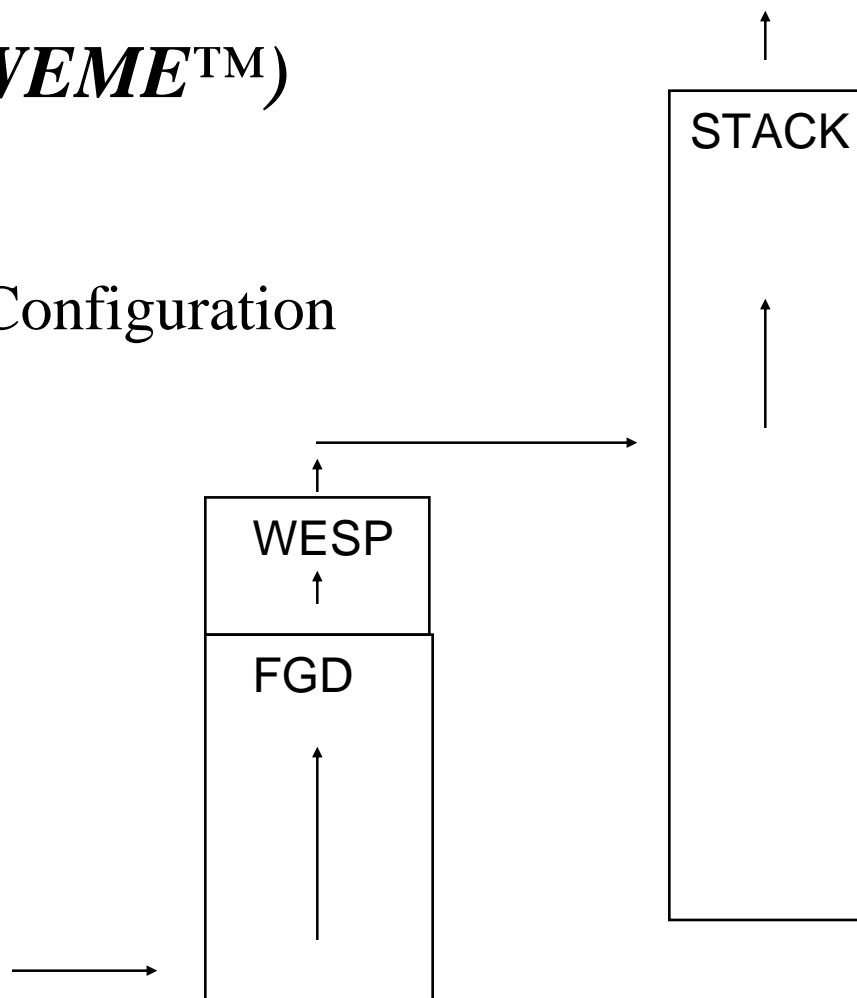
- Mid-High Sulfur Coals (bituminous)
 - FGD System installed for SO₂ control
 - Saturated Flue Gas
 - Functions as a “Wet Electrostatic Mist Eliminator”

- Low Sulfur Coals (sub-bituminous & lignite)
 - No FGD installed
 - Unsaturated flue gas
 - High LOI &/or Elemental Hg
 - Last field after a dry ESP “Hybrid dry-wet ESP”



Wet Electrostatic Mist Eliminator (WEME™)

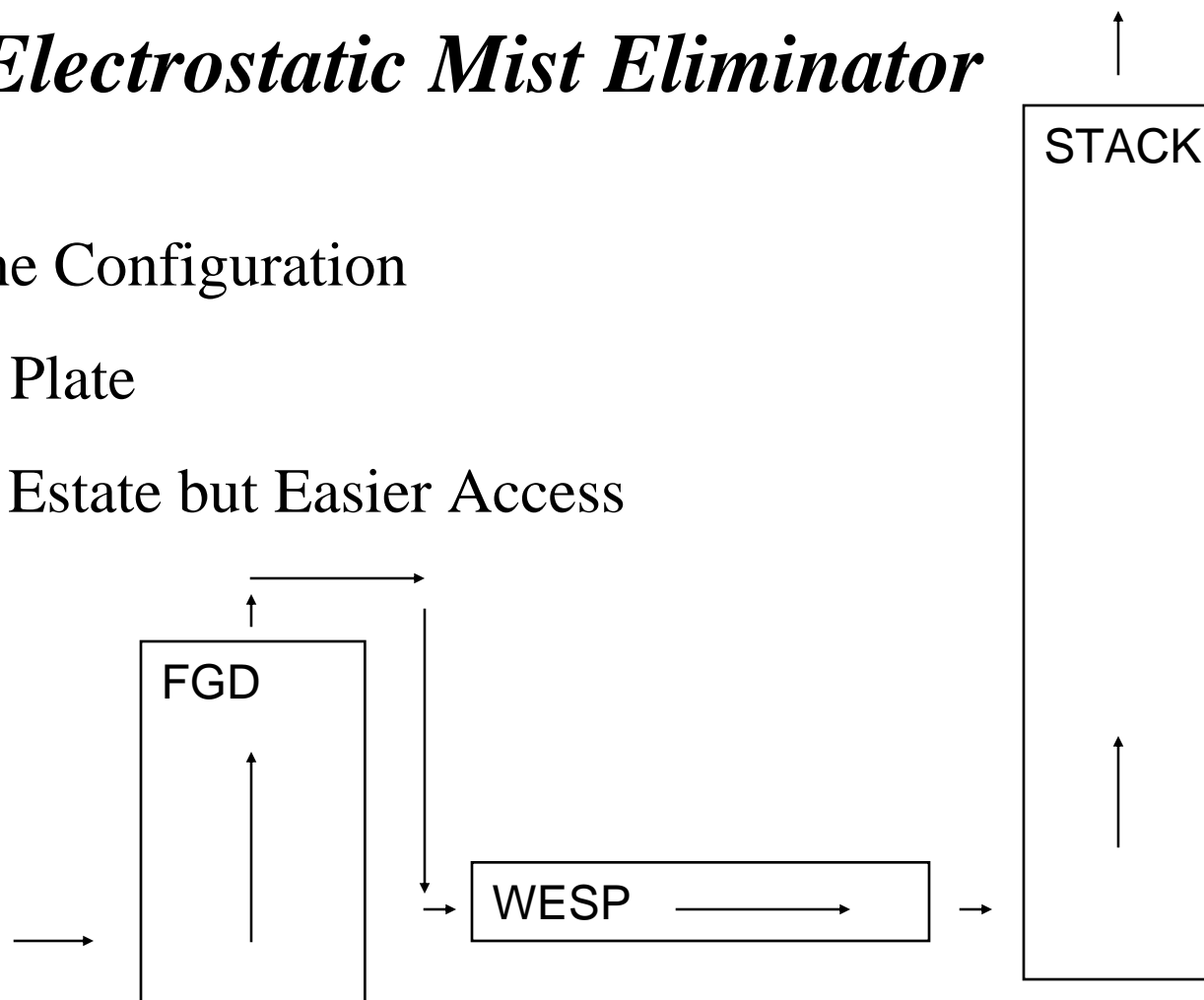
- Mounted on top of FGD
- Vertical Tubular Up-Flow Configuration
- No Additional Real Estate





Wet Electrostatic Mist Eliminator

- Stand Alone Configuration
- Horizontal Plate
- More Real Estate but Easier Access





Full Scale Installation

- Xcel's Sherco Station
- Units 1 & 2 750MW each
- Historic Opacity >40%
- 22 WESP Modules added
- New opacity <10%



First Energy's Bruce Mansfield Plant

- 3 x 800 MW Coal-Fired Units
- Mid-High Sulfur Coal
- Existing Opacity >50%
- Opacity Required <20%
- Investigated Control of
 - PM_{2.5}, SO₃, Hg
 - WESP Pilot Unit



PM_{2.5} & SO₃ Test Results

	Sept/01 1 field	Nov/01 2 fields	Nov/02 2 fields	July/03 2 fields
PM_{2.5}	79%	96%		93%
H₂SO₄	76%	92%	89%	88%

Note: WESP designed for 90% removal at 5,000 acfm

Testing performed at 8,000 acfm, 60% beyond design point



Incremental Hg Removal Across FGD & WESP

	Inlet $\mu\text{g}/\text{m}^3$	FGD outlet	WESP Outlet	Total
Hg^p	4.37	80%	76%	95%
Hg⁺⁺	6.02	69%	86%	96%
Hg⁰	2.55	-15%	18%	6%
Total Hg	12.94	62%	41%	78%

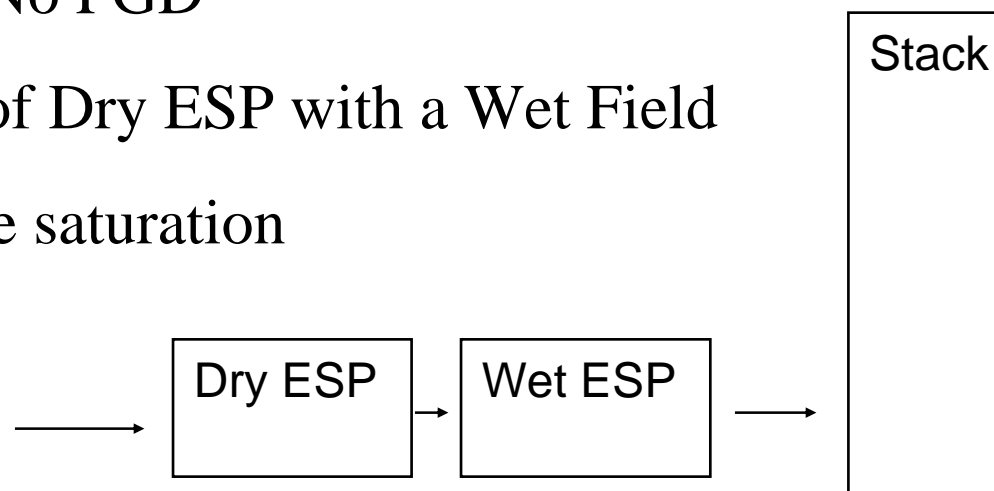


Hybrid Dry-Wet ESP™

Low Sulfur Coals-No FGD

Retro-fit last field of Dry ESP with a Wet Field

Operate 50°F above saturation



EPRI Pilot Testing-1995

Particulate matter:	95%
Sulfur dioxide:	20%
Hydrogen chloride:	35%
Hydrogen fluoride:	45%



Hybrid Dry-Wet ESP Pilot

- Alabama Power
- Plant Miller
- PRB Coal
- SCR- Dry ESP
- 2 MW Slip-stream
- Horizontal Plate WESP



Hybrid Wet ESP Pilot w/PEESP Hg Test Results

- Inlet Hg = $5.5 \mu\text{g}/\text{m}^3 - 6.3 \mu\text{g}/\text{m}^3$
- 5 Test Runs
- Total Hg Removal = 34%-51%
- No Speciated Testing Performed
- Further Testing Nov/Dec 2005



Comparison of Dry vs. Wet Approach

Dry Approach

Dry Scrubber/Baghouse

- Higher pressure drop-filters
- More fan capacity
- Flue gas above saturation -more volume
- Limited Coal Sulfur Content
- Dry waste by-product
- Larger volume of waste
- No water treatment required
- Higher operating cost

Wet Approach

Wet Scrubber/Wet ESP

- Lower pressure drop-open design
- Less Fan capacity
- Cools Flue gas to saturation - less volume
- Applicable for High Sulfur Coals
- Wet waste by-product
- Waste treated & concentrated
- Wastewater treated & recycled
- Lower operating cost



WESP Conclusions

- **Old, well-established technology**
- **Primarily for PM_{2.5} & SO₃ control**
- **High Removal Efficiencies –up to 99%+**
- **Opacity Reduction to <10%**
- **Offers Additional Hg, metal & SO₂ control**
- **Used on Mid-high sulfur coals with saturated flue gas**
- **Used on Low-sulfur coals with unsaturated flue gas**
- **Various Types & Configurations**
- **Low Pressure drop, maintenance & small footprint**
- **Improvements are reducing size, cost & Hg emissions**



**Wheelabrator
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THANK YOU

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