

# Mercury Issues for ESP/FF Technology

*WPCA/Dominion Seminar*

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# Some Basics...

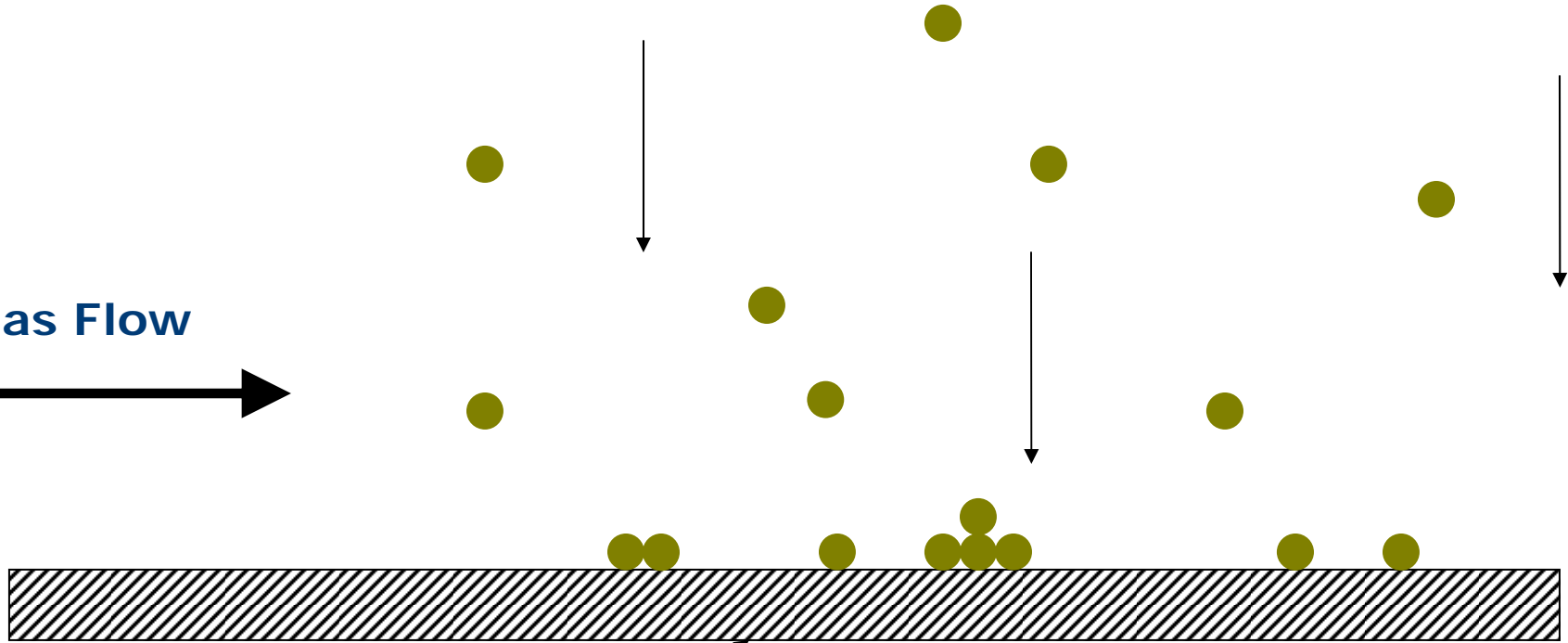
## ESPs

- Creates Residence Time
- Exposure of Hg to gas constituents
- Small Temp. change
- Some ash/gas contacting

## Fabric Filters

- Creates Residence Time
- Exposure of Hg to gas constituents
- Small Temp. change
- Intimate ash/gas contacting

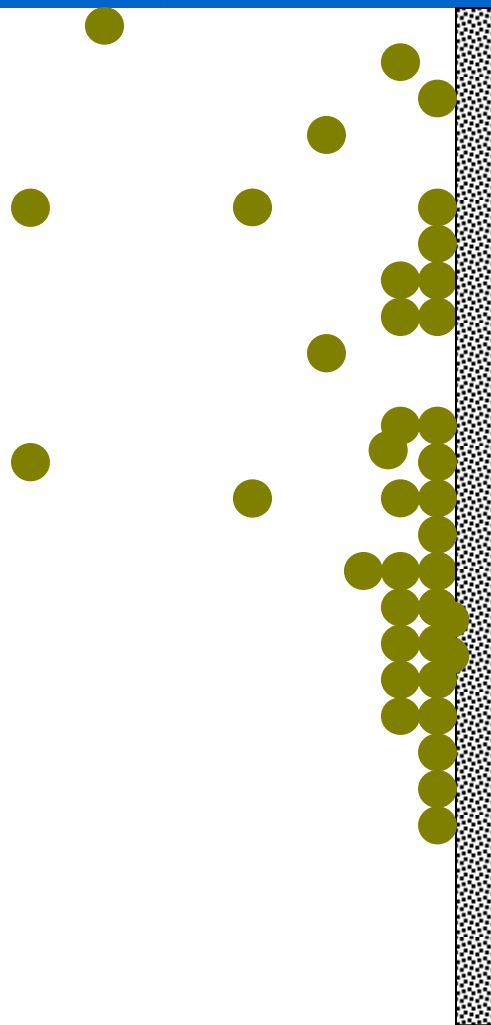
Gas Flow



Precipitator Plate

# ESP PHYSICS

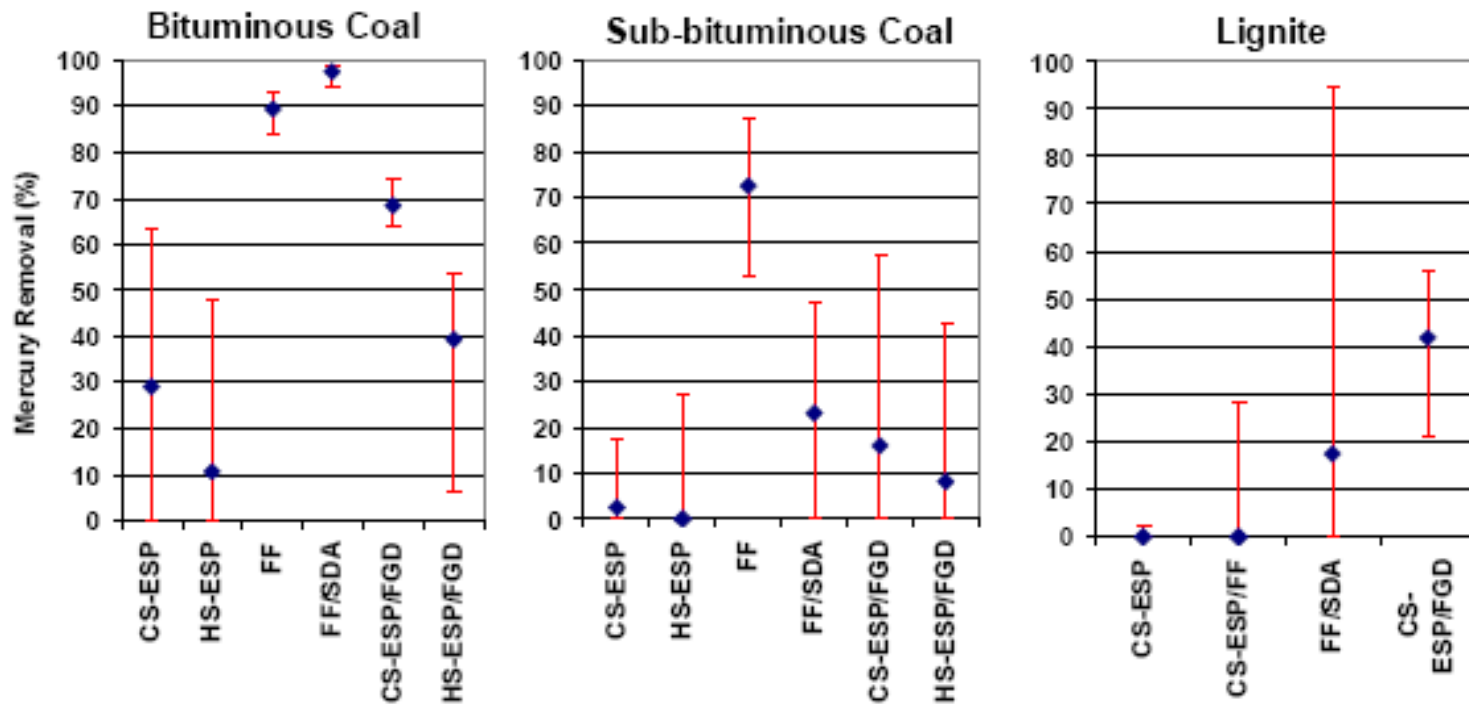
Gas Flow



Fabric

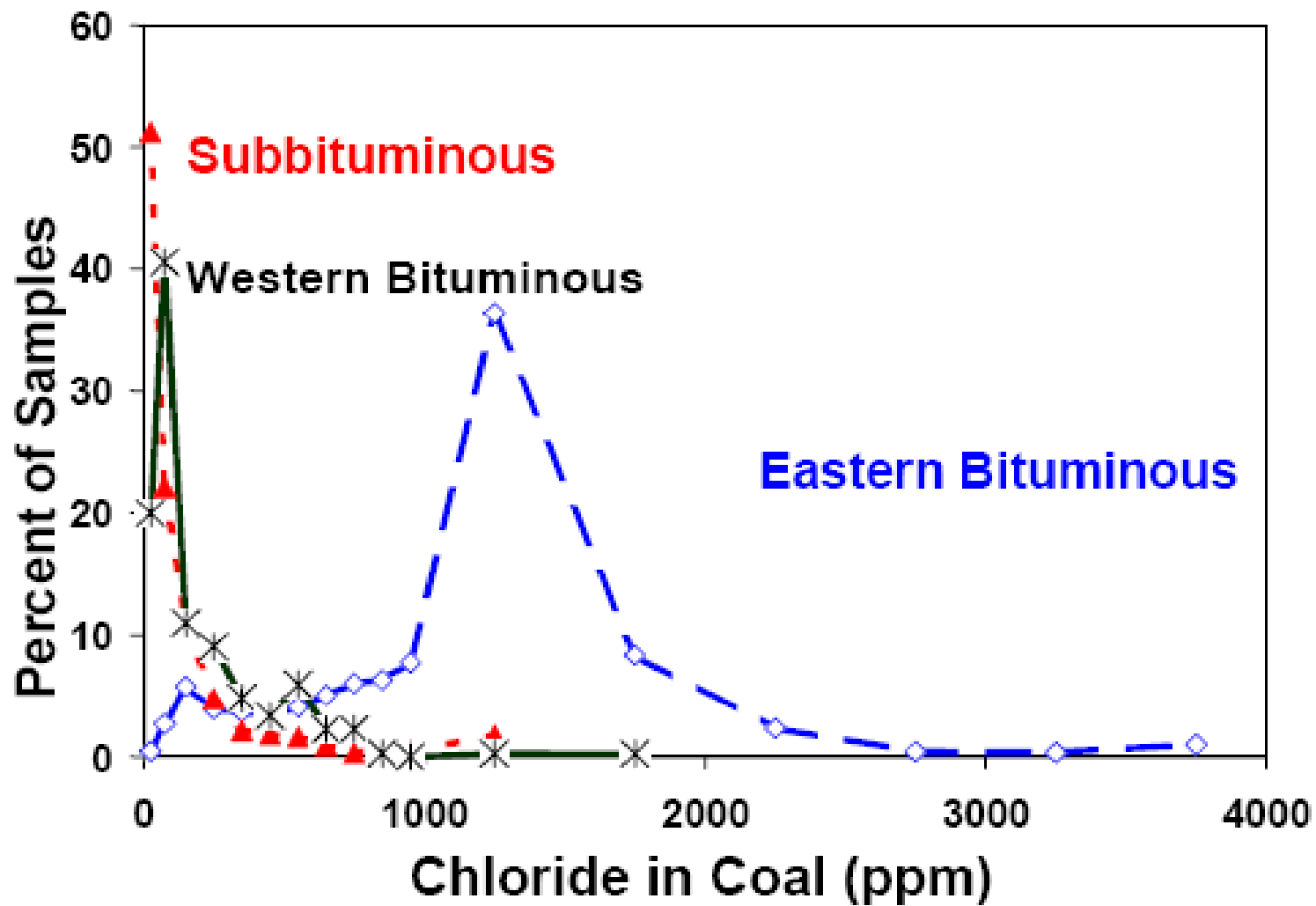


**FF PHYSICS**



# Native Control Effectiveness

-For Illustrative Purposes Only – All Individual Devices Vary ! -



**Distribution of Chloride in Coal by Type**

**Speciated Mercury Measured by Ontario Hydro Method, Baseline Conditions  
(Without Sorbent Injection). Average of Three Runs, Brayton Point Unit 1, June 2002.**

	<b>Particulate (<math>\mu\text{g}/\text{dncm}</math>)</b>	<b>Elemental (<math>\mu\text{g}/\text{dncm}</math>)</b>	<b>Oxidized (<math>\mu\text{g}/\text{dncm}</math>)</b>	<b>Total (<math>\mu\text{g}/\text{dncm}</math>)</b>
ESP Inlet	4.6	ND <0.21	0.26	5.1
ESP Outlet	<0.007	ND <0.29	0.18	0.48
Removal Efficiency (%)	99.8	N/A	30.8	<b>90.6%</b>

Note: all mercury numbers are  $\mu\text{g}/\text{dscm}$  at 32°F, 3% O<sub>2</sub>.

**Example of High Native Hg Removal - ESP**

**Speciated Mercury Measured by Ontario Hydro Method, Baseline Conditions.**

<b>Location</b>	<b>Particulate (<math>\mu\text{g}/\text{dncm}</math>)<sup>1</sup></b>	<b>Elemental (<math>\mu\text{g}/\text{dncm}</math>)<sup>1</sup></b>	<b>Oxidized (<math>\mu\text{g}/\text{dncm}</math>)<sup>1</sup></b>	<b>Total (<math>\mu\text{g}/\text{dncm}</math>)<sup>1</sup></b>	<b>Total (lbs/TBtu)</b>
ESP Inlet	1.97	12.22	2.51	16.7	12.2
ESP Outlet	0.01	9.80	6.01	15.8	11.5
<b>Average RE %</b>	<b>99.5</b>	<b>19.8</b>	<b>-139.3</b>	<b>5.3</b>	
% of Total at Inlet	11.8	73.1	15.0		
% of Total at Outlet	0	61.9	38.0		

*Note 1: Normal: T = 32°F, Values corrected to 3% O<sub>2</sub>*

## Example of Low Native Hg Removal - ESP



**Pre-Baseline Mercury Measurement Results (S-CEM).**

<b>Location</b>	<b>Total Mercury <math>\mu\text{g}/\text{dNm}^3</math> @ 3% <math>\text{O}_2</math></b>	<b>Oxidized Mercury %</b>
ESP Inlet	7–10	5–33
ESP Outlet/COHPAC <sup>®</sup> Inlet	7–10	29–51
COHPAC <sup>®</sup> Outlet	7–10	52–76
Mercury Removal Across ESP		0%
Mercury Removal Across COHPAC <sup>®</sup>		0%

**Example of No Native Hg Removal – ESP & FF**

**Table 1. Non-Scrubbed Units with Cold-Side ESPs**

ID*	NOx Control	FGC	SCA	ESP Inlet Temp	Coal Chloride	Ash LOI	% Hg on Filter	% Hg Removal
B-1	LNB		290	289	882		0	8
B-2	LNB		550	310	575	5-10	36	26
B-3	LNB		550	245	966	3-7	30	23
B-4	LNB		252	322	2100	5-10	29	24
B-5	LNB		346	321	800	5-10	75	30
B-6	LNB&S NCR		475	262	264	25	84	88
B-7			323	320	333	3-6	60	46
L-1	LNB		599	368	18		0	7
L-2			267	395	115	1.4	17	-2
L-3				368	29		5	-1
L-4	LNB		470	329	74	1-5	1	-4
S-1		SO <sub>3</sub>	468	291	100	<.5	2	-35
S-2	OFA	SO <sub>3</sub>	686	306	57	0.09-0.18	1	-3
S-3	CC		213	317	133	1-2	16	10
S-4	LNB		279	322	76	1-2	0	8
S-5		SO <sub>3</sub>	279					28
Mix-1	LNB		440	338	3620	<1	82	74
Mix-2			220	342	180	10-20	84	67
Mix-3			220	308	187	10-20	77	54

\*B = bituminous, S = subbituminous, L = lignite, mix = blend

## Summary Data - ESPs

**Table 2. Non-Scrubbed Units with Fabric Filters as Primary Particulate Collector**

<b>ID*</b>	<b>NO<sub>x</sub> Control</b>	<b>FF Inlet Temp</b>	<b>Coal Chloride</b>	<b>Ash LOI</b>	<b>% Hg on Filter</b>	<b>% Hg Removal</b>
B-1	LNB	340	167	10-20	76	51
B-2	LNB	299	55		80	87
B-3	LNB	307	1233		100	100
B-4	LNB	290				99
L-1		358	167	2-4	14	-21
S-1	LNB	348	100	2-4	36	82
S-2	OFA	293	<10	1-2	16	57
S-3	LNB, OFA	342		<1		72
Mix-1	LNB	314	127	20-25	2	-4

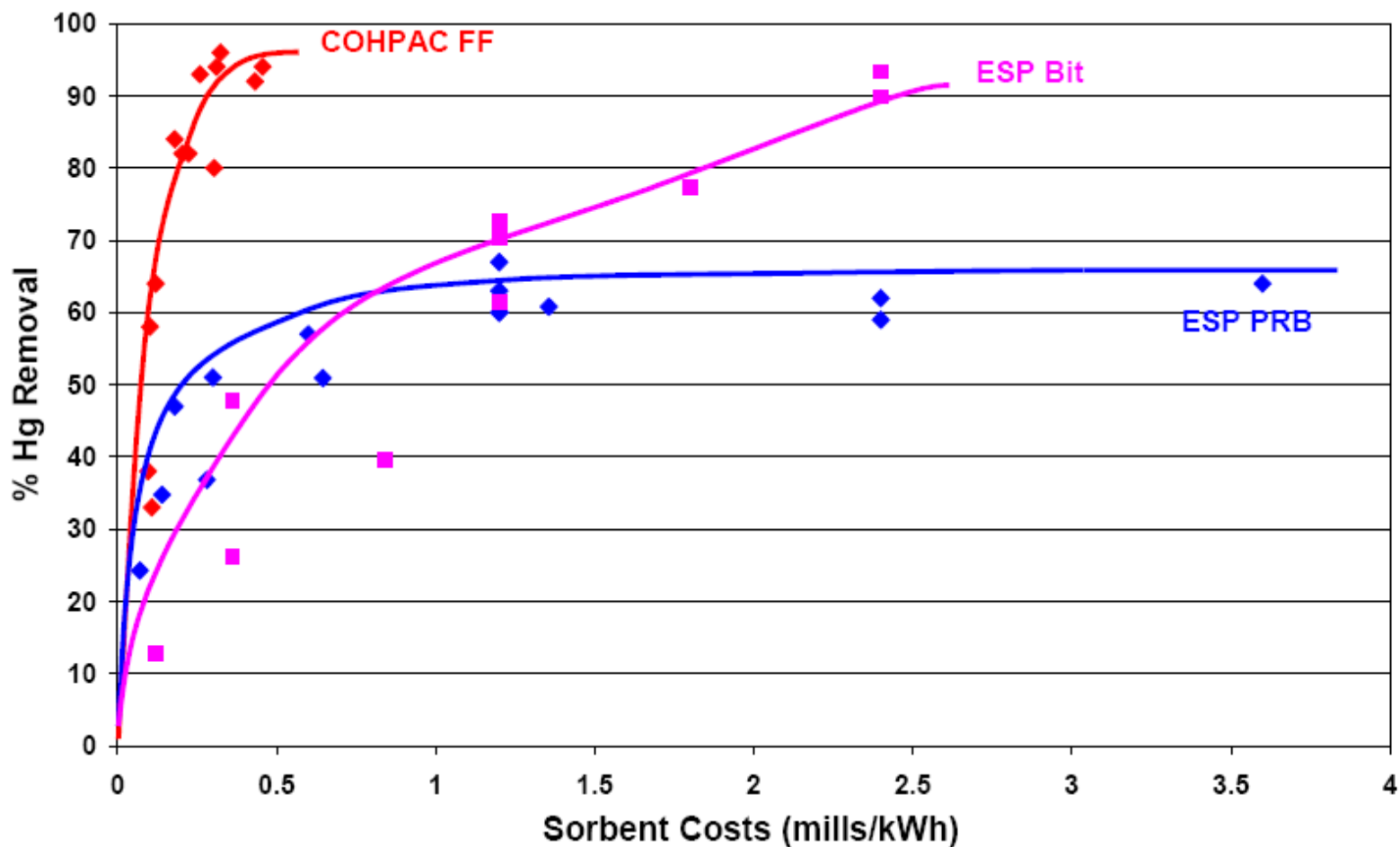
\*B = bituminous, S = subbituminous, L = lignite, mix = blend

## Summary Data –Fabric Filters

**Table 3. Summary of Average Mercury Removal in ESPs and Fabric Filters**

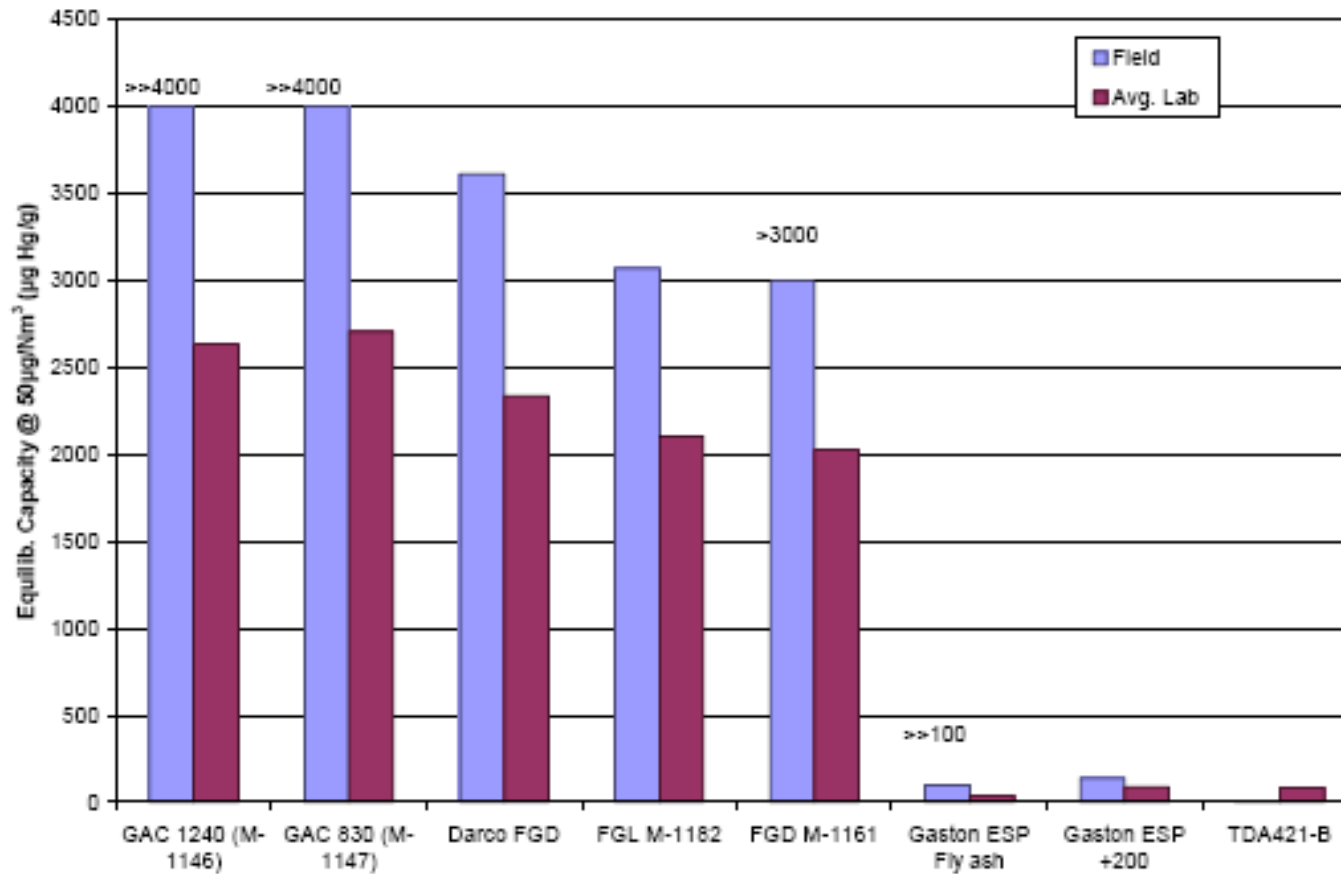
<b>Coal</b>	<b>ESPs (% Hg Removal)</b>	<b>Fabric Filters (% Hg Removal)</b>
Bituminous	35	84
Subbituminous	9	70
Lignite	2	0
Bit/Sub/Pet Coke Mix	66	NA

**Average Hg Removal Efficiencies**

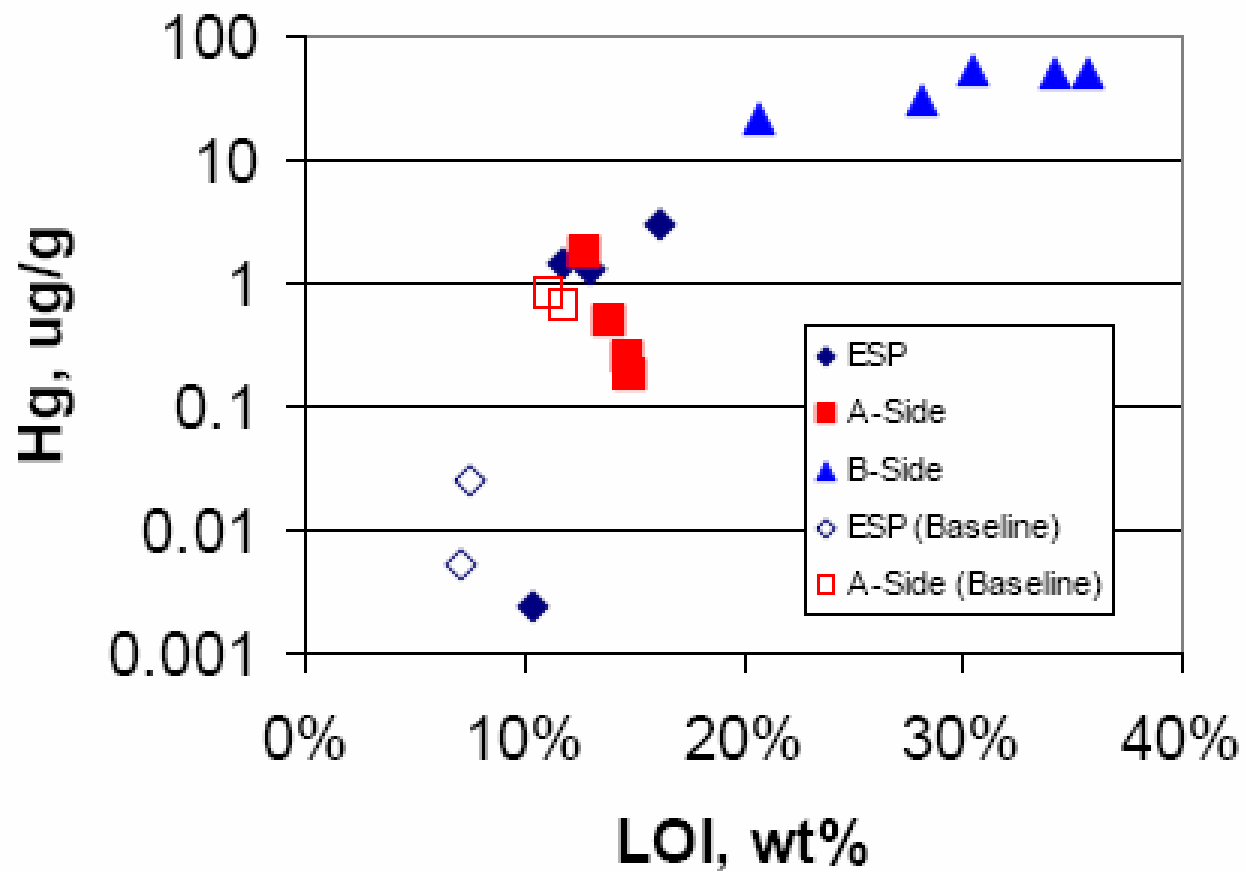


**Dramatic Effect of Sorbent Use on Hg Removal**

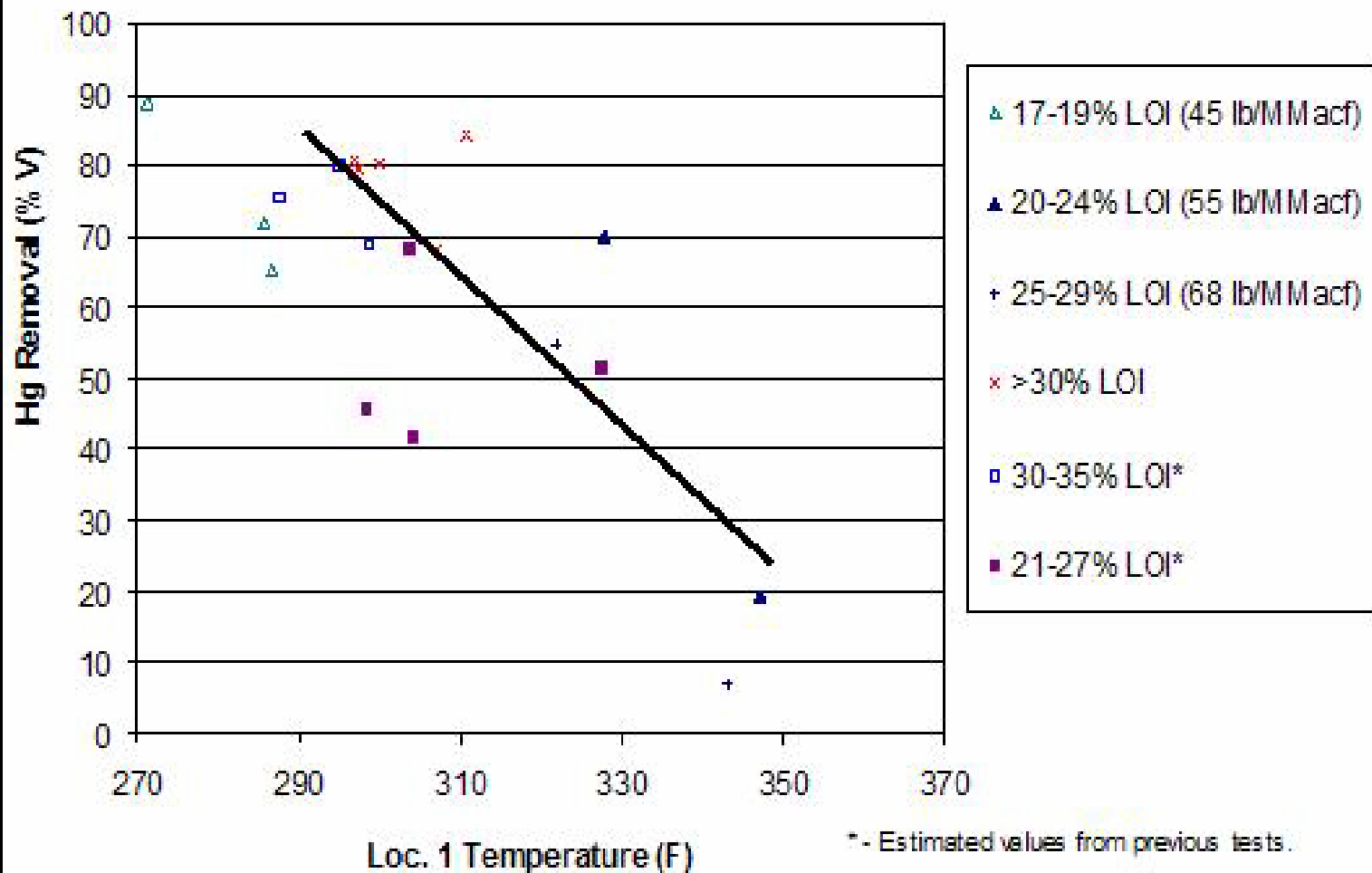
Equilibrium Adsorption Capacities for Various Sorbents Tested at 275°F  
 Gaston Station Unit 3B Cohpac Inlet - January 25-29, 2001



## Sorbent Compared to Fly Ash for Hg Removal



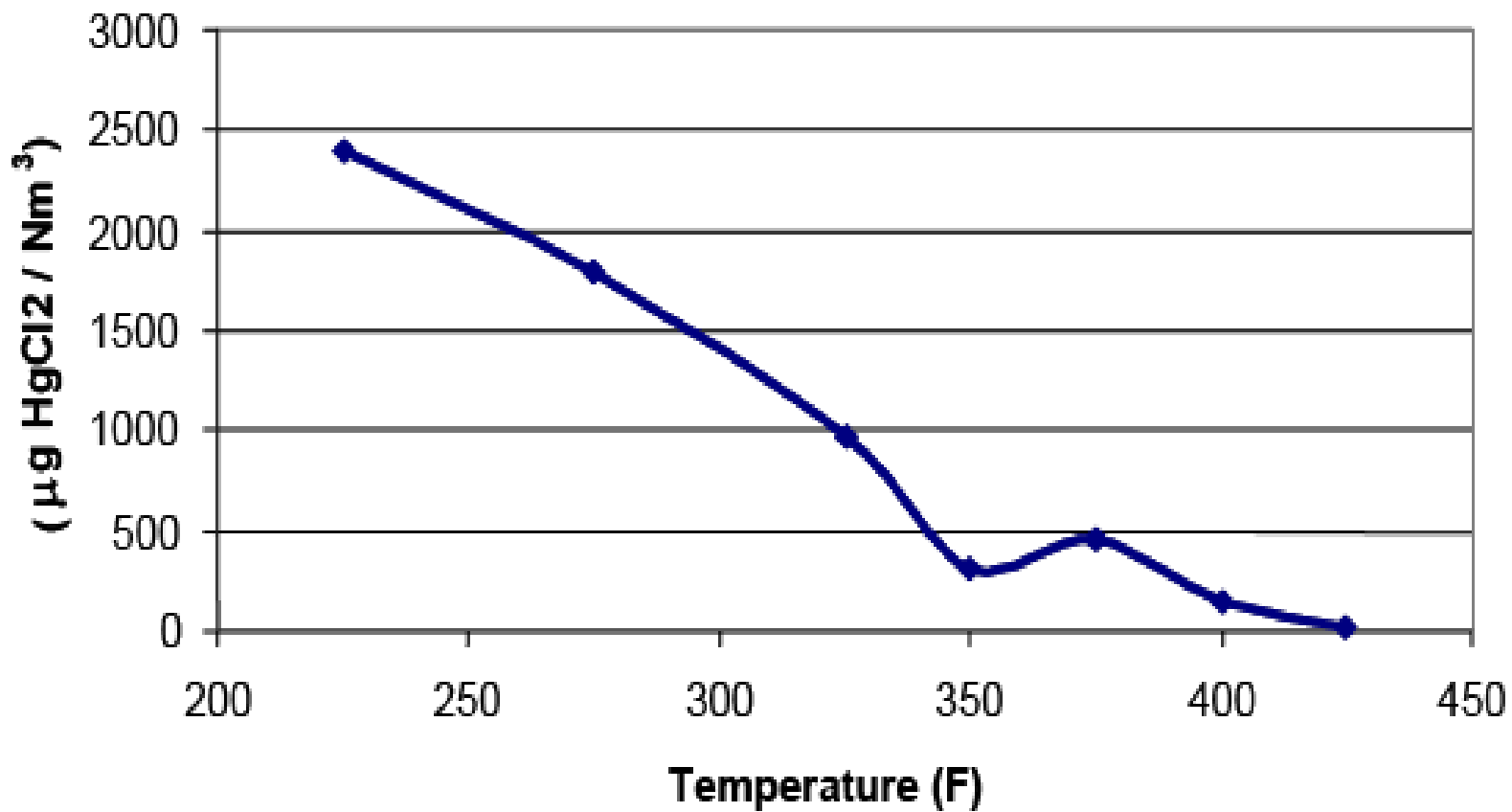
**Effect of LOI in Ash on Hg Uptake**  
Hot-Side ESP Example



# Effect of LOI and Temperature on Hg Removal

## Cold-Side ESP Example





**Sorption Capacity vs. Temperature**

**Results from Sorbent Screening Tests Conducted by URS Corporation (February 2002)**

<b>Sample Name</b>	<b>Base</b>	<b>Ads. Capacity SO<sub>3</sub> Off @ 50 mg/Nm<sup>3</sup></b>	<b>Ads. Capacity SO<sub>3</sub> On @ 50 mg/Nm<sup>3</sup></b>
Norit FGD	Lignite	4314	1380
Norit FGL	Lignite	4281	694
Donau GAL	Lignite	-	1745
Donau HOK300	Lignite	4786	-
Advanced Fuel Research – 2	Tire Derived	-	538
CarboChem	Bituminous	1948	-
SAI-B	Bituminous	1799	-
SorbTech-I	?	62	-
SorbTech-L	Lignite	2091	-
STI 020115-2	BP ash, 80% carbon	>109	0
STI 020121-3	SH ash, 80% carbon	245	0
AANP Zeolite	-	-	7

**Detrimental Effect of SO<sub>3</sub> on Sorbent Capacity**

# CONCLUSIONS

- Both ESPs and Fabric Filters can remove Hg.
- Hg Removal Efficiencies are extremely variable and site specific.
- Many factors affect Hg removal including boiler, fuel, operations, residence time, and equipment design.
- Both ESPs and FFs can be integrated into sorbent-based Hg control strategies.
- All other factors being equal – Fabric Filters generally provide better gas/particulate contacting than ESPs.

*Data presented acquired from DOE, ADA, URS.*